



#### Welcome to our webinar!

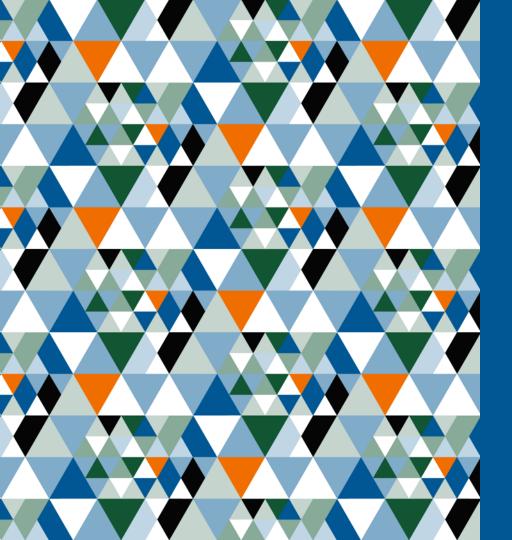
- Duration of the webinar, including the Q&A: 50 60 minutes
- Q&A:
  - Please submit your questions through "Ask a question" tab
  - Please note that the tab is not visible in the full screen mode
  - We will answer questions at the end of the webinar
- Slides: We will provide you webinar slides and the recording about one week after the live webinar



### **Agenda**

- Introduction Pekka Pohjanne, Lead, Materials for new energy technologies, VTT
- Water Electrolysis for Green H2 Production Technical Challenges, Materials and Research Activities at VTT Ville Saarinen, Senior Scientist, D.Sc. (Tech.), VTT
- Integrity of pressure vessels and pipes for H2 transportation and storage Sebastian Lindqvist, Senior Scientist, D.Sc. (Tech.), VTT
- Material challenges related to the use of hydrogen and ammonia as fuel Elina Huttunen-Saarivirta, Research Professor, D.Sc. (Materials Science), VTT
- Live Q&A





#### Introduction

Pekka Pohjanne, Lead, Materials for new energy technologies



### VTT – beyond the obvious

VTT is a visionary research, development and innovation partner for companies and society and one of the leading research organisations in Europe.

Our role is to promote the utilisation and commercialisation of research and technology in business and society. Through science and technology, we turn global challenges into sustainable solutions for business and society in a responsible way.

261 M€

turnover and other operating income

2,213

employees

43%

of the net turnover from outside Finland

32%

a doctorate or a licentiate's degree

**Establishment year** 

1942

Steered by Ministry of Economic Affairs and Employment of Finland



Hydrogen (in the) economy

 A vision of a large-scale switch to using hydrogen as an energy carrier

Eternal "magic bullet" in energy scenarios

Main advantage is its versatility

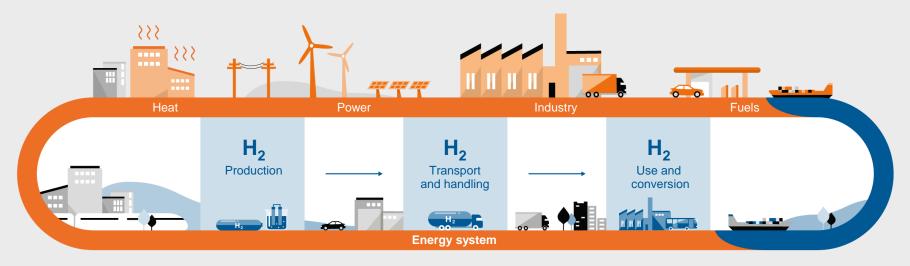
Can be produced from a wide variety of resources

Can be used in a wide range of applications





### Hydrogen is a foundation for green industrial revolution



At VTT, we help companies explore the possibilities of hydrogen technology in their operations throughout the value chain.



### VTT will have one of the leading clean energy transition research facilities in Europe

Clean energy pilot platform in VTT Bioruukki will be built in 2022-2025.

End-to-end research facilities for carbon neutrality in transport and industries.

Innovation platform for new solutions for hydrogen, electrification and renewable fuels.

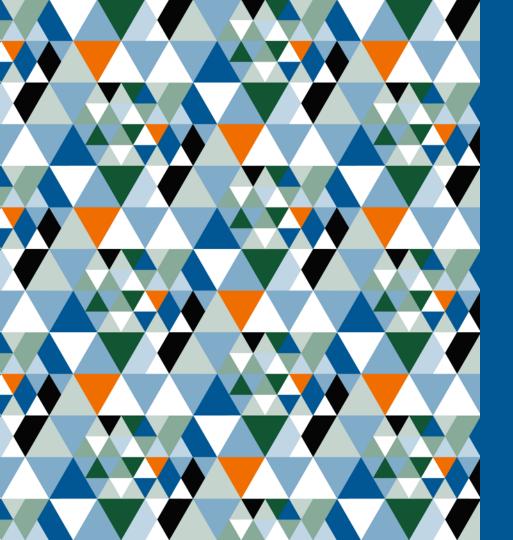




### Thank you!

Pekka Pohjanne pekka.pohjanne@vtt.fi +358 50 359 7171





### Water electrolysis for green hydrogen production

- Technical Challenges, Materials and Research Activities at VTT

Ville Saarinen, Senior Scientist



### VTT Hydrogen production and applications

- 20 years of active history in PEMFC, SOFC, and electrolysis
- ~50 person involved in H<sub>2</sub> related activities at VTT
- Mainly working with European and Finnish companies in EU-projects and contract research, currently coordinating 7 EU-projects and participating in 17 projects
- All activities are supported by validated modeling tools (CFD, thermal, mechanical, etc.) from single components to complete systems
- Excellent know-how, research facilities, wide international partner network and long experience on high temperature electrolysis and fuel cells
- Product development for Industrial partners: sales and licensing IPR for Finnish and European companies
- https://www.vttresearch.com/en/ourservices/fuel-cells-and-hydrogen





5.5.2023 VTT – beyond the obvious

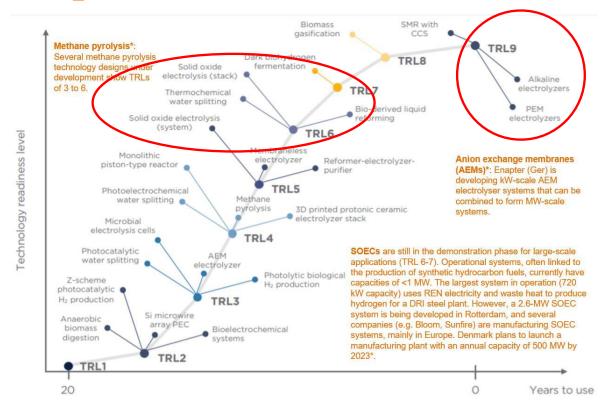


### Water electrolysis technologies

	Alkaline electrolysis (AEL)	Proton Exchange Membrane electrolysis (PEMEL)	Solid Oxide Electrolysis (SOEC)	
Reactions	C: $2 H_2 0 + 2 e^- \rightarrow H_2 + 2 OH^-$ A: $2 OH^- \rightarrow 0.5 O_2 + H_2 O + 2e^-$	C: $2 H^+ + 2 e^- \rightarrow H_2$ A: $H_2 0 \rightarrow 2 H^+ + 0.5 O_2 + 2 e^-$	C: $H_2O + 2 e^- \rightarrow H_2 + O^{2-}$ A: $O^{2-} \rightarrow 0.5 O_2 + 2e^-$	
Electrode catalysts	C: Ni or PGM A: metal oxide(s)	C: Pt A: Iridium oxide	C: Ni A: metal oxide(s)	
Electrolyte	Aqueous (KOH)	Solid (polymer membrane)	Solid oxide (YSZ)	
Temperature	30-90 °C	20-100 °C	600-900 °C	
Advantages	TRL 9, non-noble catalysts, long lifetime, relatively low-cost, MW range stacks	TRL 9, High current density, rapid system response, compact system design, pressurization	Highest efficiency, non-noble catalysts, co-electrolysis, CHP, reversible operation	
Drawbacks	Low current densities, corrosive liquid electrolyte	Pt (high price), Iridium (low availability)	TRL 7, small module size, no pressurization	



### H<sub>2</sub> production technology readiness



Source: Columbia
SIPA (Aug 2021):
Green hydrogen in a
circular carbon
economy:
Opportunities and
limits; IEA (Oct
2021)\*: Global
Hydrogen Review
2021



### SoA Electrolyser technology comparison

	AEL	PEMEL	SOEC
Electrical energy consumption* [kWh <sub>el</sub> / kg H <sub>2</sub> ]	53-60	53-65	42-45
Maximum module size	~100 MW	~20 MW	~200 kW
Cold start duration [min]	40-120	5-10	600+
H <sub>2</sub> outlet presure [bar <sub>abs</sub> ]	1-30	1.5-30	~1
Stack life time (h)	~90 000	~60 000	~20 000
CAPEX**(1 MW size) [€ / kWh <sub>el</sub> ]	400-1500	800-2000	1500-2500

<sup>\*</sup>  $H_2$  HHV= 39.4 kWh/kg, LHV= 33.3 kWh/kg

<sup>\*\*</sup> Excl. installation, grid connection, external compression, purification and storage



### Solid oxide electrolyser (SOEC) operation principle

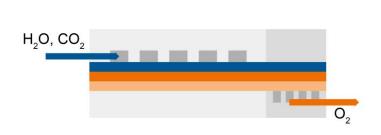
- Steam electrolysis
- $H_2O \to H_2 + \frac{1}{2}O_2$

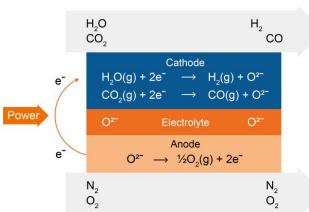
 $\Delta H \approx 250 \text{ kJ/mol}$ 

Co-electrolysis

$$H_2O + CO_2 \rightarrow H_2 + CO + O_2$$

 $\Delta H \approx 525 \text{ kJ/mol}$ 



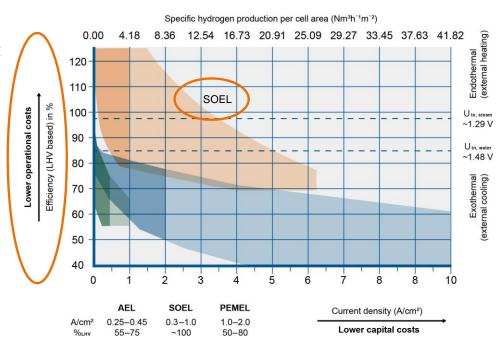


Simplified figure of SOEC cell structure



#### Efficiency can be improved without tradeoff

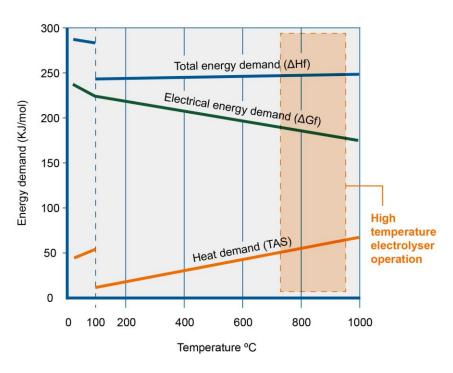
- Efficiency can be increased by
  - electrolyte and separator development (thinner, higher conductivity, better durability)
  - catalyst development (higher activity, better durability)
  - Reactant and product transport improvement (flow field, transport layer)
- Continuous field of development
- No theoretical limitation on efficiency (except energy balance)



Summary of efficiency and operational range of AEL, PEMEL and SOE cells or stacks. (Buttler & Spliethoff, 2018).



### Benefit of high temperature electrolysis originates from thermodynamics



- Lower activation losses at lower current densities at high temperatures (700-800 °C) lead to **lower power** consumption during hydrogen production
- No need for noble metal catalysts
- Solid oxide cells and stacks can be made with low cost raw materials (suitable for mass manufacturing)



#### Solid oxide technology

- High operation temperature: 600-850 °C
- SOE technology offer the potential for highest electrical efficiency in electrolysis mode (80-90%) compared to other electrolyser technologies
- SOEC technology is reversible: the same system can work both as a fuel cell and an electrolyser depending on power generation and grid stabilisation needs
- SOEC has capability also for co-electrolysis of steam and CO<sub>2</sub>, which enables more efficient power-to-X, if integrating SOEC as part of industrial processes
- The most commercial electrolysers are nowadays alkaline, but process has low efficiency due to needed high operation voltage. PEM based technology is more expensive than alkaline and it has also its own limiting factors like availability of iridium catalyst





#### VTT SOFC/SOEC research infra

- 2 single cell test stations for SOFC/SOEC
- 5 test stations for < 3 kW SOFC/SOEC stack</p>
- 2 test stations for < 10 kW SOFC/SOEC stack</p>
- 1 SOFC/SOEC system for 2 x 10 kW
- Hydrogen quality and purity analysis
- All test stations designed and built by VTT
  - Reliable and flexible platform, long-term testing
- Specific test benches for materials and experimental facilities from stack materials to complete systems
- Currently we are developing and demonstrating SOFC and SOEC technology with our customers and partners







### **SOEC** research and publications at VTT

- A lot of SOEC related research has been done at VTT during last 15 years, more specific SOEC material characterization, performance and durability analysis [1,2] and most recently SOEC system level studies [3].
- VTT press release and Tekniikka & Talous articles

[1] J. Tallgren, O. Himanen, M. Noponen, Experimental Characterization of Low Temperature Solid Oxide Cell Stack, ECS Transactions 2017, 78, 3103.

[2] M. Kotisaari, O. Thomann, D. Montinaro, J. Kiviaho, Evaluation of a SOE Stack for Hydrogen and Syngas Production: a Performance and Durability Analysis, Fuel Cells 2017, 17, 571.

[3] Saarinen, V., Pennanen, J., Kotisaari, M., Thomann, O., Himanen, O., Iorio, S. D., Hanoux, P., Aicart, J., Couturier, K., Sun, X., Chen, M., & Sudireddy, B. R. (2021). Design, manufacturing, and operation of movable 2 x 10 kW size rSOC system. Fuel Cells, 21(5), 477-487.









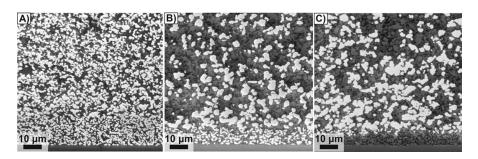
### VTT Fuel cell and electrolyser characterization solutions

- World-class characterization facilities for fuel cell and electrolyser materials, stacks, system components, and systems
- Extensive hands-on experience of working with a very broad spectrum of fuel cell related technologies
- Tailored test campaign and recommendations for solving issues specified by the customer
- Complete, fully automated fuel cell stack and system characterization facilities.
- Very wide range of test capabilities from cold climate tests to impurity sensitiveness and detailed electrochemical characterization





### Research example - SOE degradation mechanisms

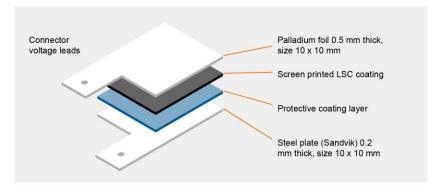


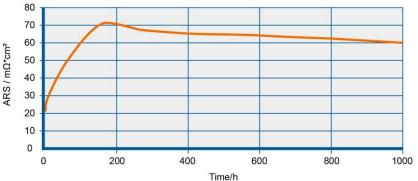
- Ni migration (function of current density, overpotential at cathode, steam content)
  - Stabilization with impregnation and formation of nanoparticle of gadolinia stabilized ceria
- Anode delamination.
  - Most critical with outdated LaSrMnO<sub>3</sub> anode, less with LaSrCoO<sub>3</sub>
- Pore formation in the electrolyte
- Thermal stress, electrocatalyst poisoning (Cr, Si),



### Research example - Characterisation of SOE interconnect coatings

- Coated steel sample is stacked adjacent to thin palladium foils with screen-printed cathode material (here LSC).
- The measurement setup introduces the following benefits:
  - Realistic electric contact between coating and cathode material with same chemical interactions as in the stack
  - Palladium spacer allows for post-test SEM/EDS analysis of Cr migration through coating into cathode material as all possible Cr in LSC originates from the sample





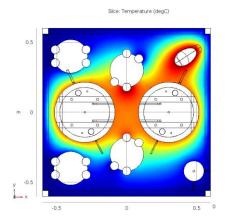
J. Tallgren et al. 2015. Evaluation of protective coatings for SOFC interconnects. ECS Transactions 68(1), 10.1149/06801.1597ecst.

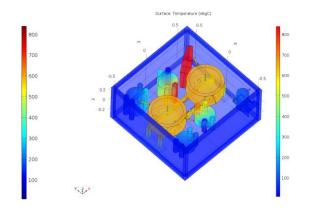
J. Tallgren et al. Comparison of different manganese-cobalt-iron spinel protective coatings for SOFC interconnects. Proc. 12th European SOFC & SOE Forum 2016



Research example – rSOC pilot system «RESSU»

- Highly instrumented Reversible SOC System Unit "RESSU" designed and build by VTT
- High efficiency and suitable for integration with various energy sources and P2X, adaptability to local energy needs (supports grid stabilisation with high penetration of renewable electricity)
- Good technology base for green, flexible and efficient energy systems





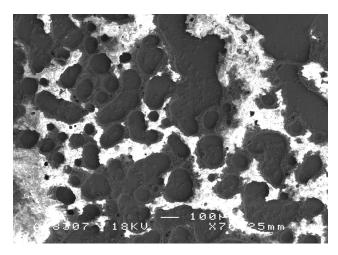


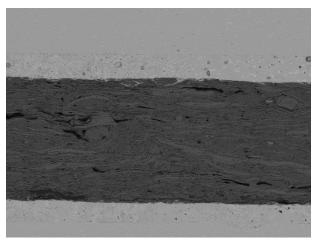
Saarinen, V., Pennanen, J., Kotisaari, M., Thomann, O., Himanen, O., Iorio, S. D., Hanoux, P., Aicart, J., Couturier, K., Sun, X., Chen, M., & Sudireddy, B. R. (2021). Design, manufacturing, and operation of movable 2 × 10 kW size rSOC system. Fuel Cells, 21(5), 477-487



### Research example: Post-mortem analysis of electrolyser system components

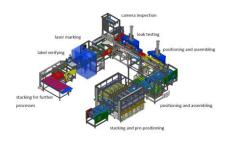
- Degradation analysis of electrolyser materials and components (cells, stacks, sealings, interconnect plates, etc)
- A wide variety of analysis services available (SEM/EDX/WDX, SIMS, etc)

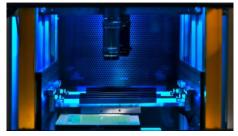






#### Research example – qSOFC







- Automated mass-manufacturing and quality assurance of SOFC stacks
- Reduction of stack production cost to 1000 €/kW at 10 MW/year volume
- Increase of production yield in all parts of stack manufacturing value chain to above
   95% by automation and quality assurance



















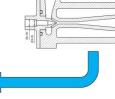


### PEM system and H2 quality research

- VTT has over 20 years of experience in PEMFC material, stack and system development. Participated in several PEMFC stack development projects
- Capability to characterize PEMFC stacks from up to 100 kW power range, both short term and long term measurements. Fuel cell systems up to 320 kW can be characterized at -32 °C...+50 °C +, also vibration, shock and drop testing.
- In system R&D, focus on contaminants from hydrogen, air and BoP components
- Cold climate issues and freeze testing at system
- At the BoP component level focus is in
  - ejector and ejector control system development,
  - air filter characterization
  - humidifier characterization









## Research example – H<sub>2</sub> quality research at VTT

- Objective: To solve the hydrogen quality for transportation applications
  - Effects of the hydrogen supply chain derived contaminants on the fuel cell systems in automotive applications
  - Recommendations for current ISO 14687 standard
  - Technical data on fuel composition on HRS
  - Establish three European laboratories, capable of measuring all of the contaminants according to ISO 14687
- Measurements with CO and CO with CO2 (combined effect)
  - The use of 13CO for contamination studies (oxidation rate monitoring with 13CO2)
- LOHC toluene (and benzene) impurity measurements
- 3-year EU-funded (FCH JU) project, coordinated by VTT. Six European leading FC research centres and independent European automotive stack manufacturer.

hydraite.eu



### Collaboration examples with VTT

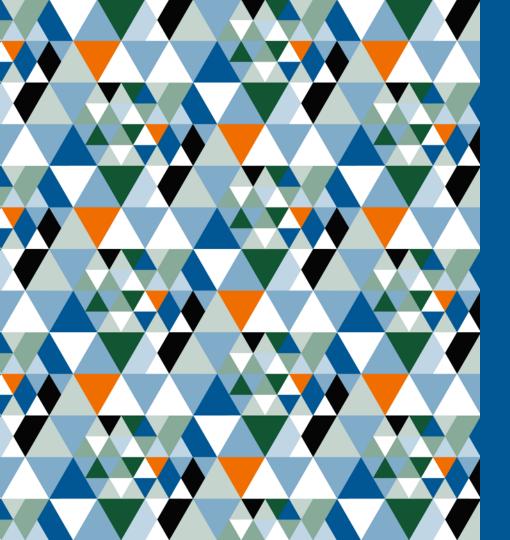
- Support in quotation requests, collaboration with electrolyser suppliers
- VTT has close dialogue with all the major electrolyser suppliers
- Networking and funding applications (>1-10 MEur bids)
- Techno-economic analysis & business case
- Demonstration activities
- Status report on the technology
- System modeling and experimental characterization



### Thank you!

D.Sc (Tech.) Ville Saarinen ville.saarinen@vtt.fi +358 40 620 2933





# Integrity of pressure vessels and pipes for H2 transportation and storage

<u>Sebastian Lindqvist</u>, Senior Scientist Siddharth Suman, Pekka Pohjanne, et. al



### Hydrogen in Finland 2015: 3 Hydrogen stations (70 MPa & 35 MPa)





Arctic Driving Center, Rovaniemi, 2012

Helsinki Harbour, 2015

### Control of material performance is crucial

- H2 diffuses to stress concentrations and decreases the material performance
  - H2 at crack tip → risk of embrittlement & fast growth
  - Right type of material testing is needed in relevant conditions
- Key features in materials selection
  - Hydrogen absorption, diffusion and interaction
  - Fatigue crack initiation & growth needs to be predictable
  - Fast or time dependent fracture risks controllable
- Make the right choice:
  - · Material type, composition and microstructure
  - Strength level, ductility, flawlessness, purity
  - Material knowledge is needed



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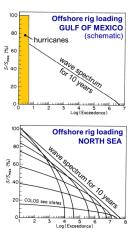
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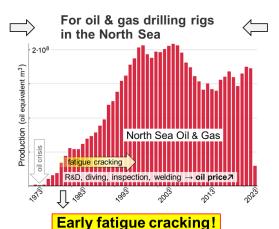


### Case example: oil drilling rigs at North Sea hydrogen into the steel by cathodic protection



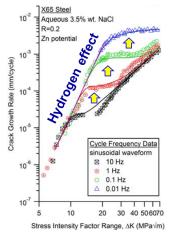


Round-the-year storming North Sea



Oil price was affected by management of hydrogen enhanced fatigue: cracking risk, inspection and repair.

#### Zn anodes for cathodic protection



#### Lessons learned:

Fatigue improvement to mitigate cracking

Optimized cathodic protection to reduce hydrogen absorption

Cathodic potential retards corrosion & crack initiation, but charges with hydrogen

and enhances crack growth

## Material selection for a new design

#### Low-alloy and carbon steels

- Risk for fast fracture depends on strength and microstructure
- For H<sub>2</sub> pressure equipment fatigue design is based on crack growth

#### Austenitic steels

- More expensive high Ni alloys (stabile austenite) are preferred
- Risk for fast fracture is generally lower

#### Non-metallic and composites

- Light weight, good corrosion resistance, low thermal conductivity
- Development towards higher pressure and large scale

#### Materials with cladding or barriers

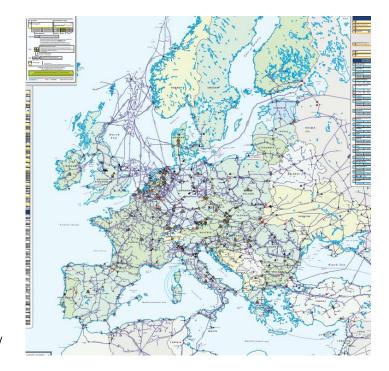
Manufacturing and inspections a challenge





## Material selection for a repurposed design

- Major interest currently: Repurposing of the European and US natural gas grid
  - Operation pressure: 40 80 bar
  - Materials: carbon steels
- What limits repurposing?
  - Knowledge of material performance
  - Knowledge of the existing condition
  - Applicability of standards
  - Mitigation measures





#### VTT's capabilities to solve material challenges of pressure vessels and pipes for H2

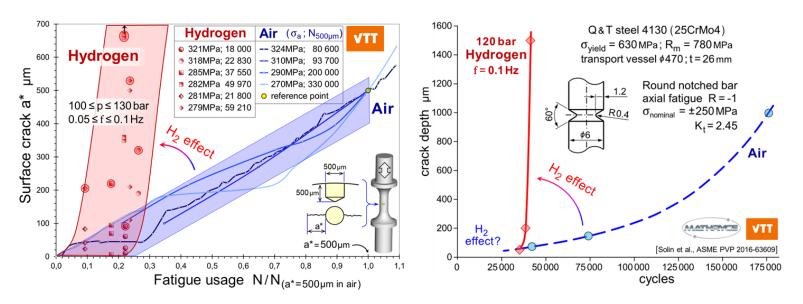
- HyBello for fatigue and fracture toughness testing in pressurized H<sub>2</sub>
  - Operational: 2014
  - Pressure: < 200 bar
  - Hydrogen charging in the future
- Quality aspects
  - Is of high importance to us
  - ISO 9001:2015
  - ISO 17025 accredited testing
  - ISO 14001:2015
  - Continues development



- 20 years of experience on hydrogen issues and even longer for developing tailored solutions for industrial purposes
- Multidisciplinary expertise
  - design, leakage, accident simulations, etc.
- Ongoing projects:
  - MASCOT 2021, MATHIAS 2023
- Active participation inside the research community
  - ASME, ASTM, ISO, etc.



#### R&D collaboration EU (FCH), U.S. DOE and Japan



VTT contributed to pre-normative R&D and recommendations for ISO in 2012-2015 on design and testing criteria for safe pressure equipment in hydrogen service.

Challenge: Conservative Fracture Mechanics → competitive design – not yet ready.

## How VTT can help you to make the right choices?

We solve your challenges related to pressure vessels and pipes for H<sub>2</sub> transportation and storage

 Right type of testing in relevant environment, under realistic loading of a real design to optimize the investment

Improved design and material selection, and selection of optimal operation conditions

 Driven to provide tailored solutions and develop methods to provide more meaningful data

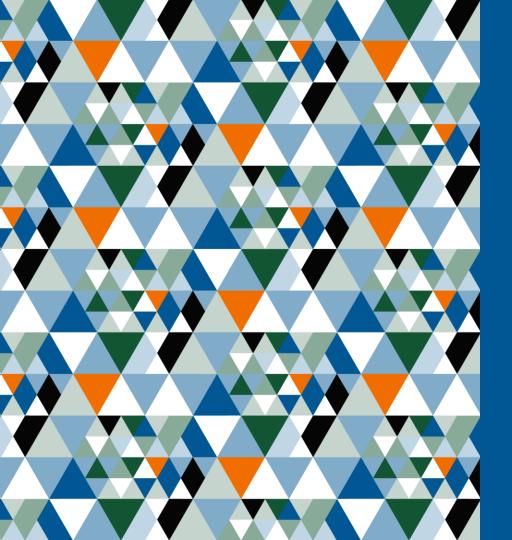




## Thank you!

Sebastian Lindqvist@vtt.fi +358 40 138 7256





## Material challenges related to the use of hydrogen and ammonia as fuel

Elina Huttunen-Saarivirta, Research Professor



#### Why hydrogen?

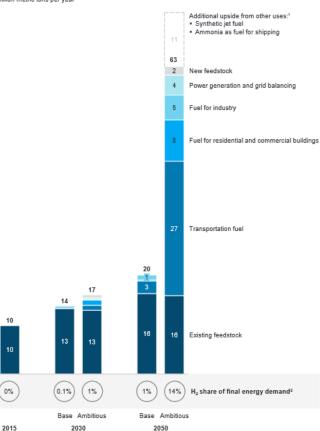






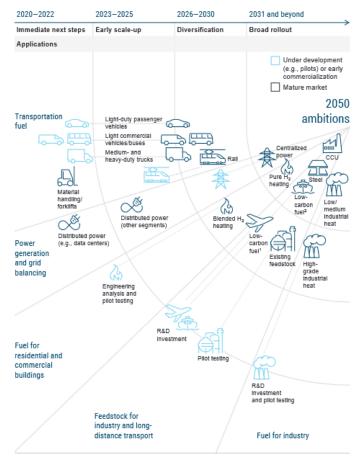


Hydrogen demand potential across sectors – 2030 and 2050 vision Million metric tons per year



From: FCHEA, Roadmap to a US Hydrogen Economy. http://www.ushydrogenstudy.org/

#### Hydrogen applications road map



<sup>1</sup> Carbon capture and utilization (for chemicals production)



<sup>&</sup>lt;sup>2</sup> Biofuel, synfuel, ammonia



#### In Finland

## Government's climate policy: climate-neutral Finland by 2035

The objective of the Programme of Prime Minister **Sanna Marin**'s Government is for Finland to be carbon-neutral and the first fossil-free welfare society by 2035. This requires even faster emissions reductions in all sectors and stronger carbon sinks.

#### Finland has a well populated value chain for hydrogen



Business Finland, National hydrogen roadmap for Finland, 2020.

## Wärtsilä gas engines to burn 100% hydrogen

Wärtsilä Corporation, Press release, 5 May 2020 at 11:00 UTC+2



The technology group Wärtsilä continues to lead the ongoing transformation of the energy and marine sectors towards carbon-free solutions through its future fuel development work. The company is pioneering the adoption of hydrogen and ammonia as viable engine fuels through advanced testing in Wärtsilä's fuel-flexible combustion engines.



#### Hydrogen as a fuel

Table $1-$ Comparison of hydrogen properties with other conventional fuels (modified from Ref. [22]).							
Fuel	HHV (MJ/kg)	LHV (MJ/kg)	Stoichiometric Air/Fuel ratio (kg)	Minimum Ignition Energy (MJ)	Auto Ignition Temperature (°C)	Combustible Range (%)	Flame Temperature (°C)
Hydrogen	141.6	119.9	34.3	0.017	585	4-75	2207
Propane	50.3	45.6	15.6	0.30	450	2.1-9.5	1925
Methanol	22.7	18.0	6.5	0.14	460	6.7-36	1870
Methane	55.5	50.0	17.2	0.30	540-630	5-15	1914
Diesel	44.8	42.5	14.5	_	180-320	0.6-5.5	2327
Gasoline	47.3	44.5	14.6	0.29	260-460	1.3-7.1	2307

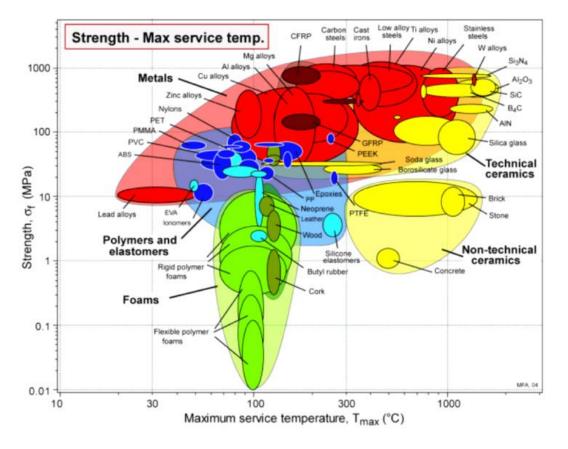
HHV: Hydrogen heating value

LHV: Lower heating value

H. Ishaq et al., Int. J. Hydrogen Energy 47, 2022, 26238-26264.

$$2H_2 + O_2 \rightarrow 2H_2O$$



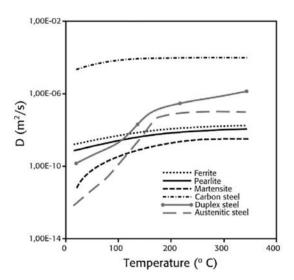


Example of materials selection chart by Ashby: strength vs. maximum service temperature.

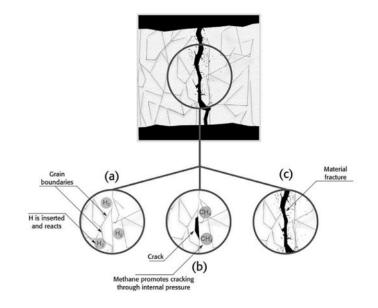


#### H<sub>2</sub> and materials at elevated temperatures

- High temperature hydrogen attack (HTHA), T>220°C
- $C + 2H_2 \rightarrow CH_4(g)$
- → Loss of ductility, i.e., embrittlement



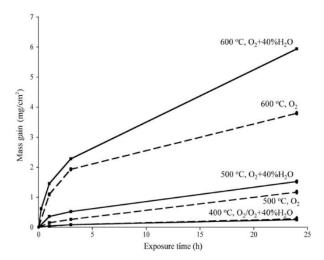
Hydrogen diffusion coefficient as a function of temperature for steel microstructures.



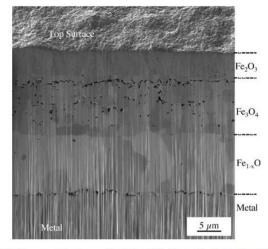


#### Oxidation of alloys in water vapour, H<sub>2</sub>O(g)

- Accelerated oxidation kinetics
- Presence of porosity & voids



**Fig. 1a.** Oxidation kinetics of iron in dry  $O_2$  and in  $5\%O_2 + 40\%H_2O + 55\%N_2$  at 400-600 °C. The vertical bars (1, 3 and 24 h) show the scatter in mass gain of the triplicate samples. The lines are just guides to the eye.



**Fig. 10.** FIB cross-section image after 24 h at  $600\,^{\circ}$ C in wet  $O_2$ . Total oxide thickness in the image is about 40  $\mu$ m. The hematite, magnetite and wüstite layers are about 6, 18 and 16  $\mu$ m, respectively. The sample is tilted 42°.

#### Oxidation of alloys in water vapour, H<sub>2</sub>O(g)

Volatile oxides, hydroxides and oxyhydroxides

$$MO_x + nH_2O(g) + mO_2(g) = MO_{(x+n+2m)}H_{(2n)}(g).$$
 (1)

For the systems of interest, here, the specific volatilization reactions are:

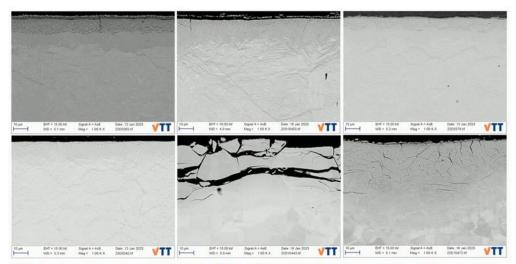
$$\frac{1}{2} \operatorname{Cr}_{2}O_{3} + \operatorname{H}_{2}O(g) + \frac{3}{4} O_{2}(g) = \operatorname{Cr}O_{2}(\operatorname{OH})_{2}(g) \\
\frac{1}{2} \operatorname{Cr}_{2}O_{3} + \frac{3}{4} O_{2}(g) = \operatorname{Cr}O_{3}(g)$$
(2)
$$\frac{1}{2} \operatorname{Cr}_{2}O_{3} + \frac{3}{4} O_{2}(g) = \operatorname{Cr}O_{3}(g)$$
(3)
$$\frac{1}{2} \operatorname{SiO}_{2} + 2\operatorname{H}_{2}O(g) = \operatorname{Si}(\operatorname{OH})_{4}(g)$$
(4)
$$\frac{1}{2} \operatorname{SiO}_{2} + \frac{1}{2} \operatorname{H}_{2}O(g) = \operatorname{Si}(\operatorname{OH})_{2}(g)$$
(5)
$$\frac{1}{2} \operatorname{Al}_{2}O_{3} + \frac{3}{2} \operatorname{H}_{2}O(g) = \operatorname{Al}(\operatorname{OH})_{3}(g)$$
(7)

E.J. Opila, Materials Science Forum 461-464, 2004, 765-774.



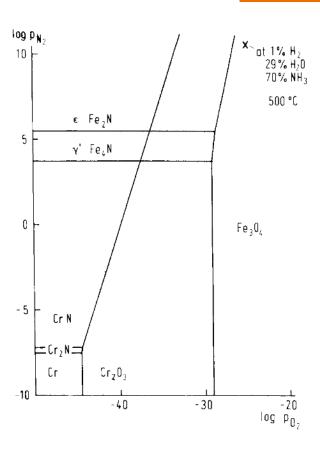
#### Nitridation by ammonia, NH<sub>3</sub> (g)

Brittleness of the formed nitride layers



SEM micrographs of the cross-section of samples in 1000h exposure of 14%NH<sub>3</sub>-Ar at 400 °C. 1000x magnification and AsB backscatter detector. Top left to bottom right: : 42CrMo4, 34CrAINi7, 34CrNiMo6, X40CrSiMo10-2, 316L and 316+.

Ongoing M.Sc. Thesis at VTT (Sofia Ojasalo)





#### **MASCOT**

#### MAterialS for CO<sub>2</sub>-neuTral processes in resource-intensive industries

- Aim is to tackle the material technology related challenges raised in emerging fossil-free processes
- Business Finland partnership project with six companies and two research institutes
- 2022 2025
- EUR 7.2 M€ total





#### **MASCOT**



www.mascotproject.fi



#### **MASCOT** collaboration key for success













Metso:Outotec

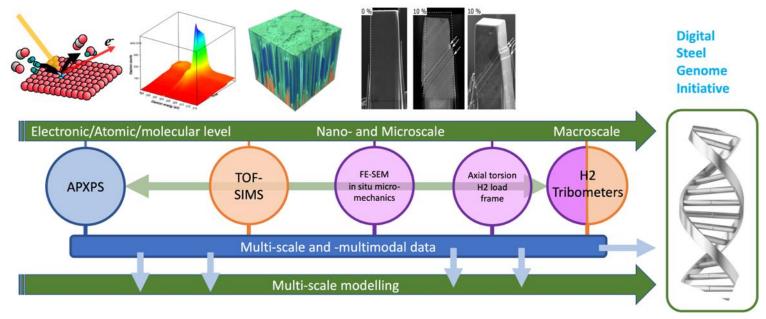






## SA FIRI: Hub for Hydrogen-Materials Interaction Research Infrastructure (H2MIRI), with OU & TAU

**Figure 2.** The multi-scale and multimodal approach of H2MIRI. The produced data is used for multi-scale modelling and as part of the Digital Steel Genome Initiative. Coordinated sample transfer systems and digital tracking allow characterization at different sites.



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## Thank you!

Elina Huttunen-Saarivirta elina.huttunen-saarivirta@vtt.fi +358 40 145 3199



#### Q&A

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  - Please note that the tab is not visible in the full screen mode



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  - Mika Malkamäki, Solution sales lead:
     Mika.malkamaki@vtt.fi
     +358405028586

# bey<sup>O</sup>nd the obvious